

Battery Technology and Simulation of Lithium-Ion Systems

A3PS

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- Motivation
- Lithium-ion batteries – key attributes
- Modeling approaches
 - Polynomial approximation
 - Equivalent-circuit models
 - Electrochemical model
- Ageing of Lithium-ion batteries
- Generic energy management
- Conclusion

Mechanical & electrical integration

- Communication interfaces
- Packaging
- HV connections
- Power interface

Thermal management

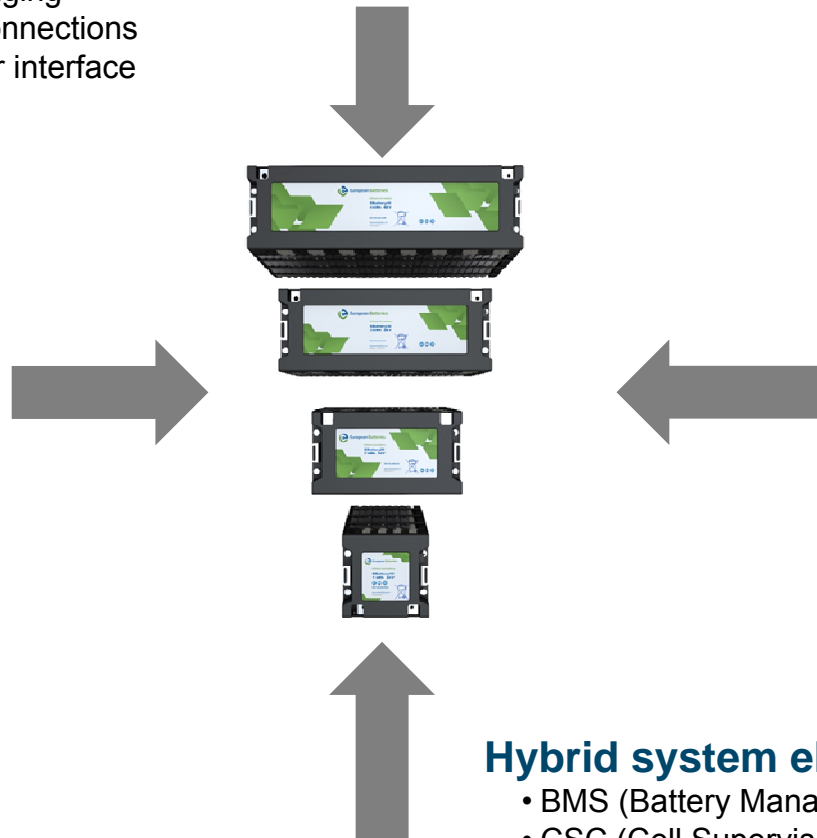
- air-cooled
- liquid-cooled

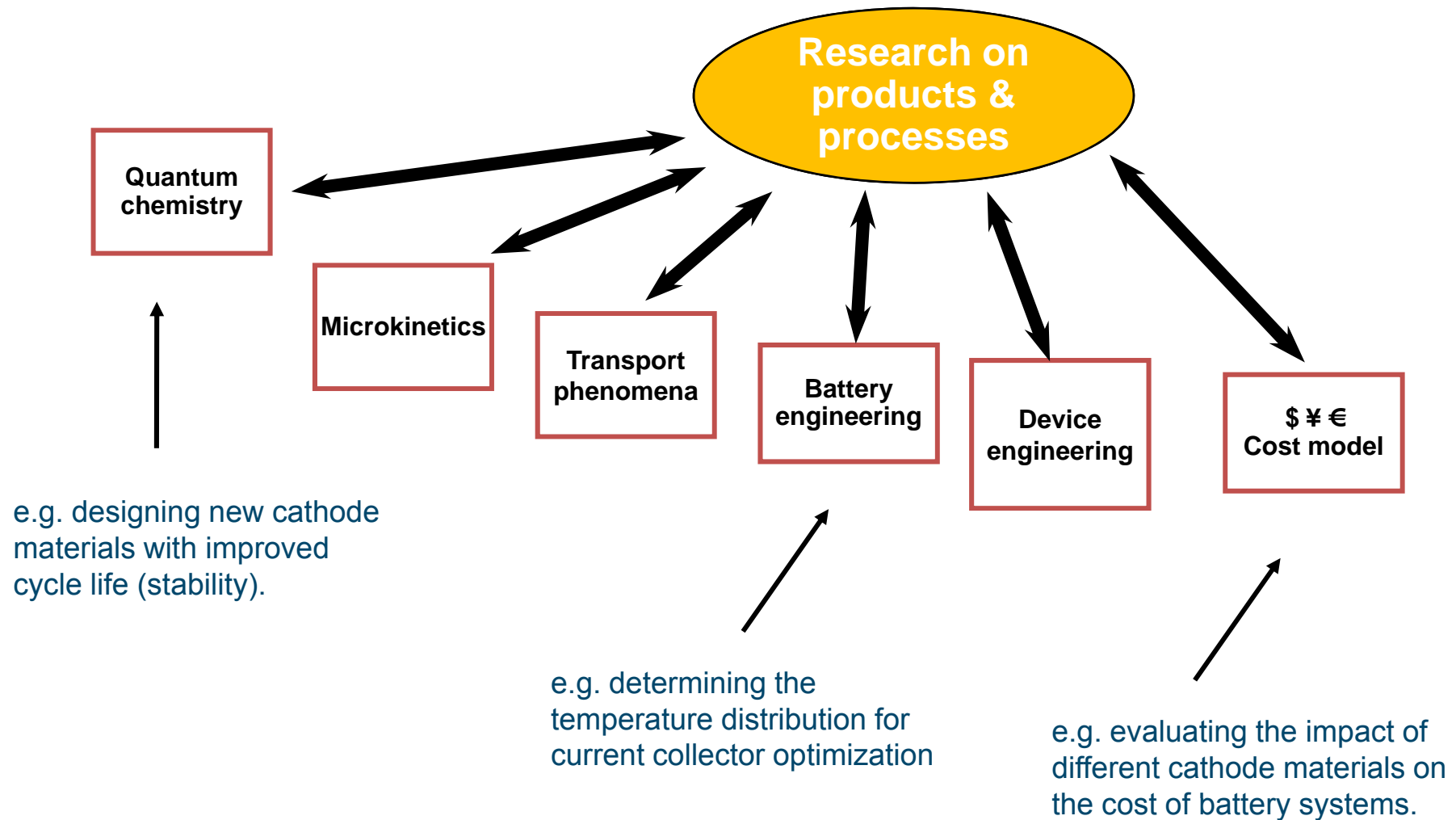
Electrochemistry

- Li-ion
- NiMH (Nickel-metal hydride)

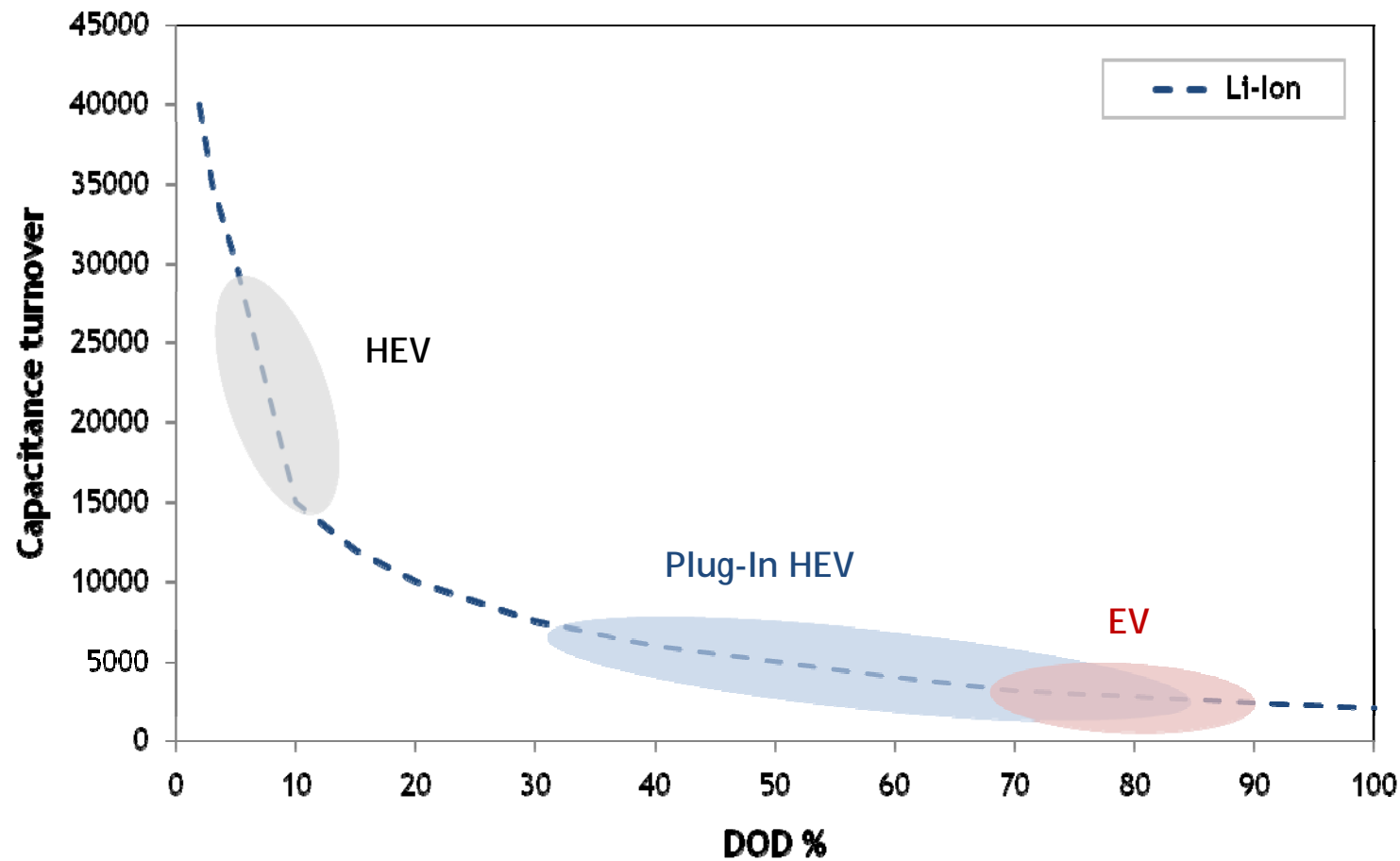
Hybrid system electronics

- BMS (Battery Management System)
- CSC (Cell Supervisory Controller)
- Software
- Electronics
- Power interface





- **Energy density**
 - Total amount of energy that can be stored per unit mass or volume. How long will your system run before it must be recharged?
- **Power density**
 - Maximum rate of discharge power per unit mass or volume. Low power: i-pod. High power: power tools.
- **Low-temperature energy and power density**
 - The amount of energy that can be recovered decreases at low temperatures due to slower charge and mass transfer.
- **Safety**
 - At high temperatures, certain battery components decompose and can cause hazardous exothermic reactions.
- **Lifetime**
 - Most applications require a high stability of energy density and power density during repeated cycling.

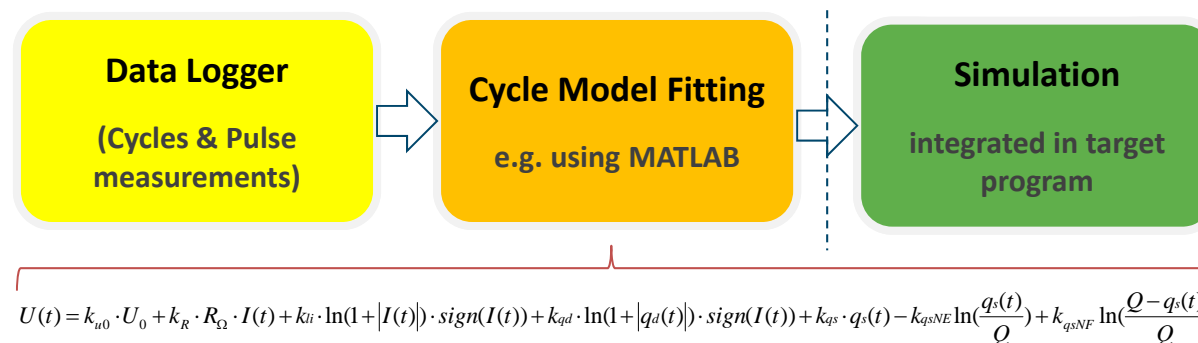


Source: Johnson Controls Saft Advanced Power Solutions GmbH

Model	Simulation speed	Accuracy	Finding parameters	Versatility	Ageing
Ideal voltage source	++	--	none	++	-
Behavioral model	+	~	+	-	-
<i>Polynomial model</i>	+	+	~	~	~
<i>Equivalent circuit model</i>	+	+	~	+	~
<i>Electrochemical model</i>	-	+	-	~	+

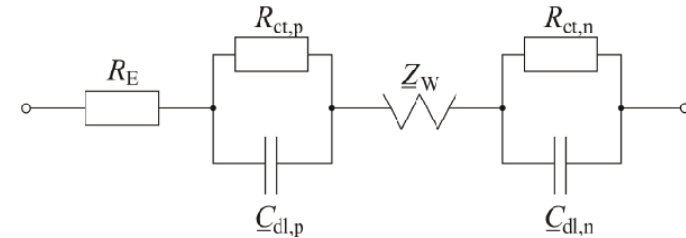
will be discussed in the following

- Thermal/electrical model
 - $U(\text{SoC}, T) = f(I(t), T, \text{SoC}, \text{SoH})$



- Objective:
 - finding a proper mathematical/empirical description of the cell behavior
- based on a designed experiment (DoE)
- Approximation of measurements or reducing a more complex model (e.g. using Padé approximation, Krylov subspaces, surrogate models, TSVD, neural networks, fuzzy rules,...)

- fast
- easy to approximate
- Double-layer capacity
- Warburg impedance
- Ageing effects (empirically, up to a certain degree)
- Problem: temperature-dependency

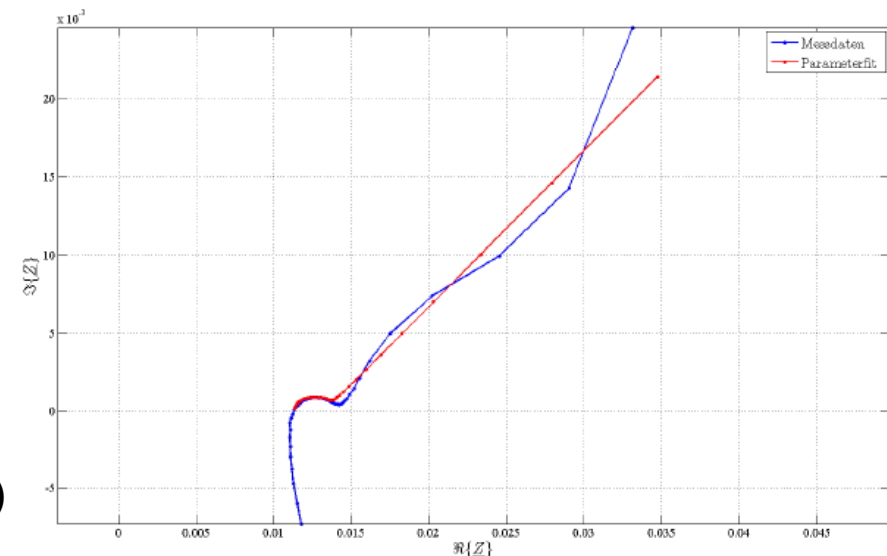


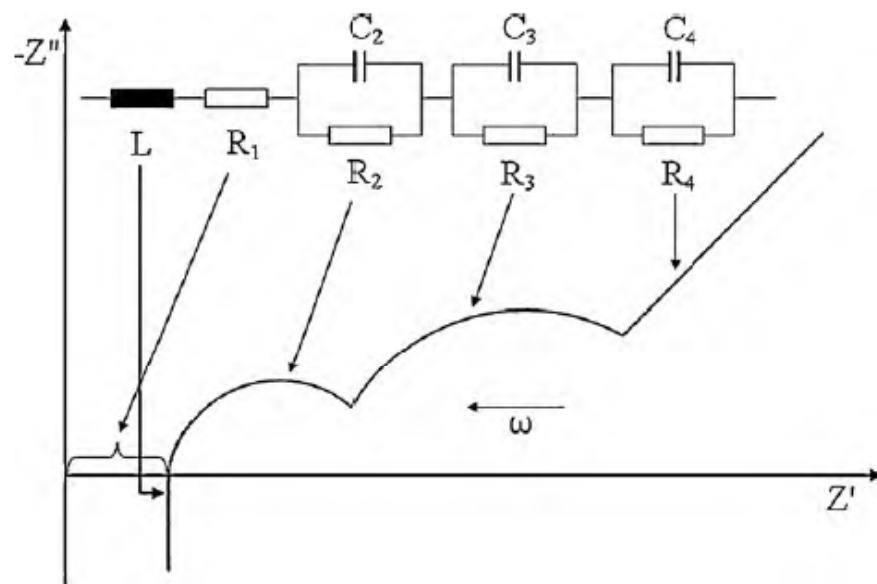
$$E(i, T, t) = \sum_{j=1}^n P_j \cdot \text{sod}^n(i, T, t) + \Delta E_0(T)$$

$$\text{sod}(i, T, t) = \frac{1}{Q_0} \int_0^t \alpha(i, t) \cdot \beta(T, t) \cdot i(t) dt$$

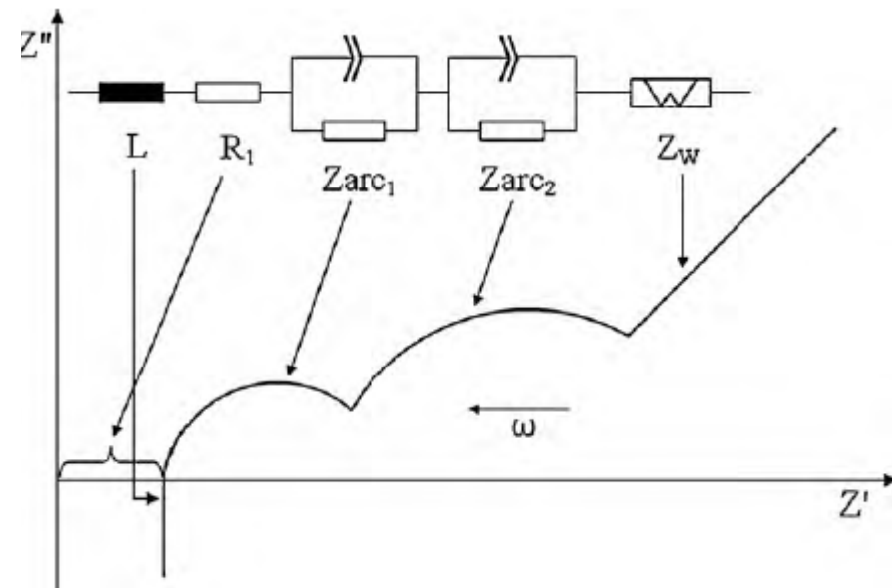
$$i(t) = \frac{E(i, T, t)}{R(t) + Z_{Load}}$$

$$c_p m \frac{dT(t)}{dt} = i^2(t) \cdot R(t) - h \cdot A \cdot (T(t) - T_{Ambient})$$





Simple equivalent circuit model
8 parameters



More advanced equivalent circuit model
26 (=2+10+10+4) parameters
 $Z_{arc} \rightarrow$ depression of semi-circles
Warburg: diffusion process (high frequencies)

Source: D. Andre et al., Jnl. of Power Sources, 2010 (in press)

Semi-circles:

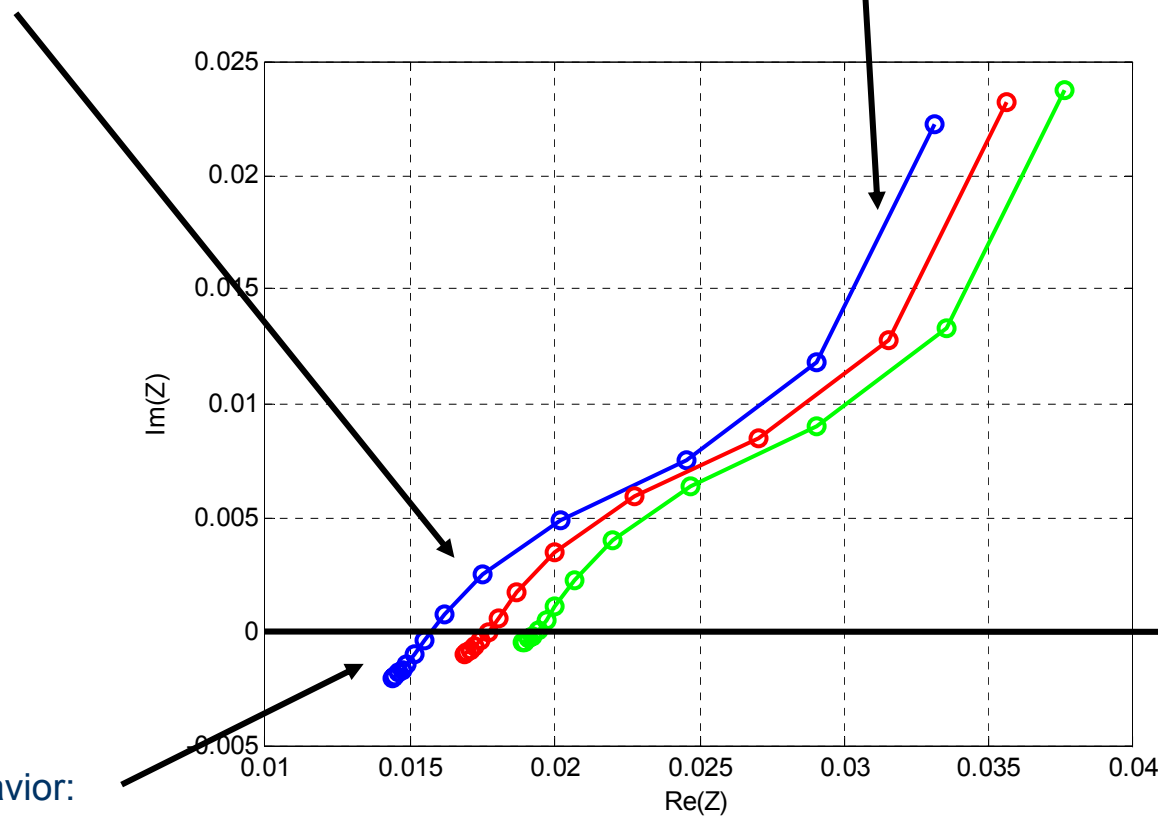
Electrochemical mechanism (reaction)

Double-layer capacity

Passivation layer at electrodes

Diffusion part:

Diffusion of lithium-ions in active mass of electrodes



Ageing

(constant temperature cycling)

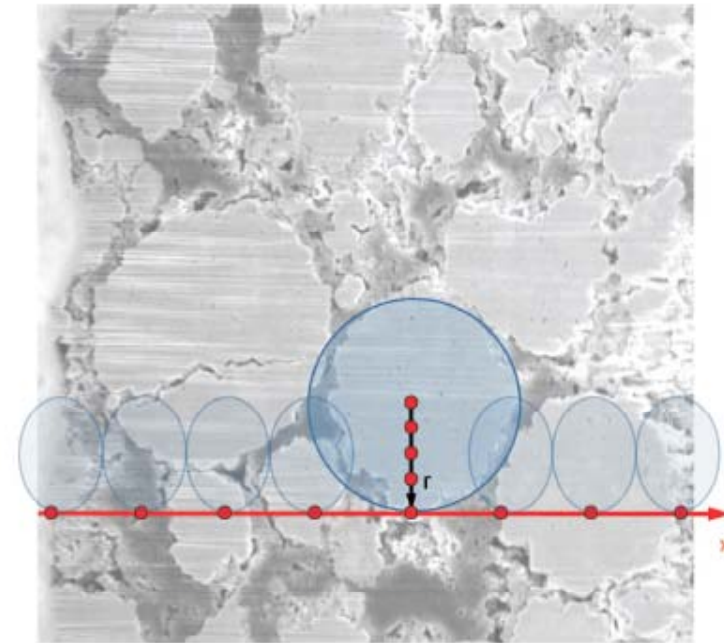
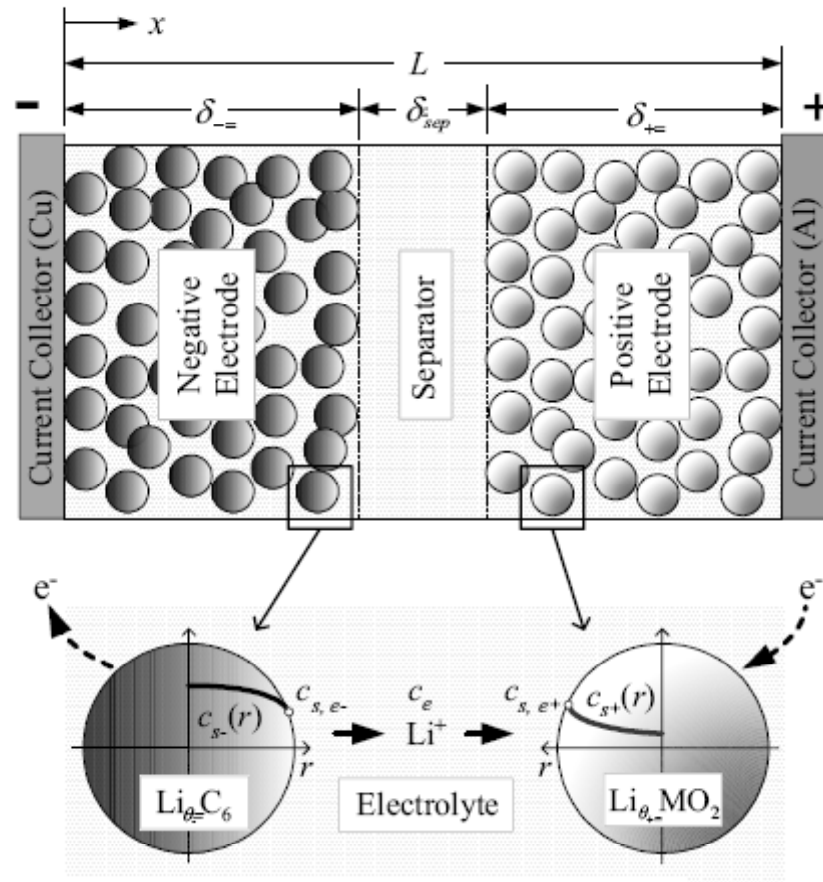
Increasing internal resistance

Zero-crossing:
Internal resistance

Inductive behavior:

Cell geometry of electrodes

Porosity of active mass

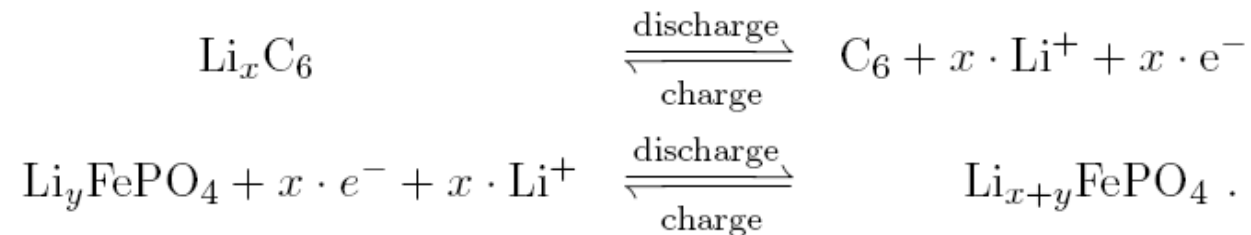


Discretization of the electrode. The main direction of electrochemical reaction is defined by x while additional diffusion in solids is described in r -direction.

Source: K.. A. Smith, IEEE Conf. on Control Applications, 2008

Source: Virtual Vehicle Research Center, 2009

- Set of coupled partial differential equations (PDEs)
- Basic electrochemical reaction (LiC_6 / LiFePO_4 Lithium-ion cell)



- Leads to (taking into account ionic and electronic conductivity)

$$\begin{aligned}
 i_1 &= -K_1^{\text{eff}} \frac{\partial \phi_1}{\partial x} \\
 i_2 &= -K_2^{\text{eff}} \frac{\partial \phi_2}{\partial x} + \frac{2K_2^{\text{eff}} RT}{F} (1 - t_+^0) \frac{\partial \ln c_2}{\partial x} \\
 i &= i_1 + i_2
 \end{aligned}$$

- Charge transfer and charge balance (**Butler-Volmer**)

$$\frac{\partial i_2}{\partial x} = j = aFk \left((c_{1,\text{surf}} - c_{1,\text{min}})^{1-\beta} e^{\frac{\alpha F}{RT}(\phi_1 - \phi_2 - E)} - (c_{1,\text{max}} - c_{1,\text{surf}})^{\beta} e^{\frac{(1-\alpha)F}{RT}(\phi_1 - \phi_2 - E)} \right)$$

$$0 = \frac{\partial i_1}{\partial x} + \frac{\partial i_2}{\partial x}$$

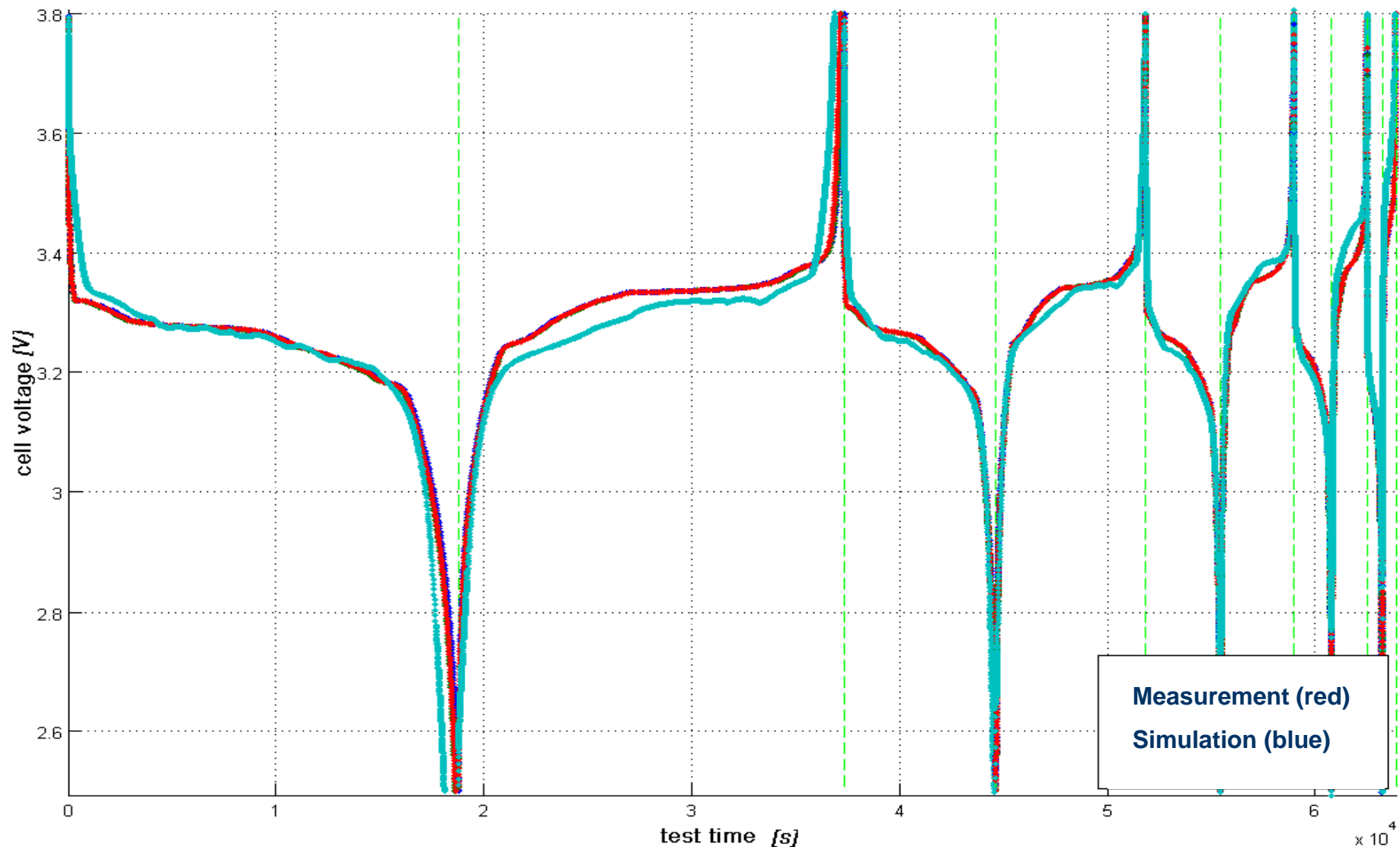
- Diffusion for solid and liquid (**Fick's law**)

$$\frac{\partial c_1}{\partial t} = \frac{1}{r^2} \frac{\partial}{\partial r} \left(D_1 r^2 \frac{\partial c_1}{\partial r} \right)$$

$$\frac{\partial(\text{eps}_2 c_2)}{\partial t} = \frac{\partial}{\partial x} \left[\text{eps}_2 D_2^{\text{eff}} \frac{\partial c_2}{\partial x} \right] + (1 - t_+^0) j$$

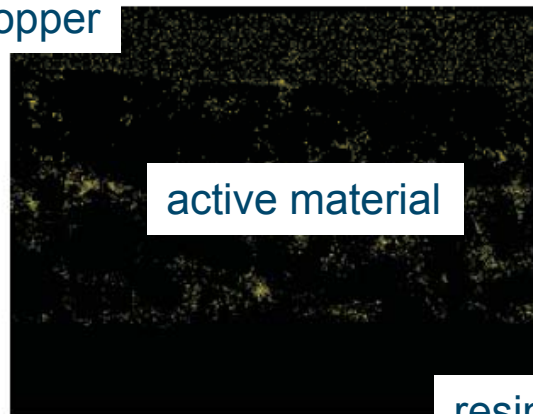
- Bruggeman relation** (porosity and tortuosity of the porous electrode materials)

$$K_1^{\text{eff}} = K_1 \text{eps}_1^{\text{brug}}, \quad K_2^{\text{eff}} = K_2 \text{eps}_2^{\text{brug}}, \quad D_2^{\text{eff}} = D_2 \text{eps}_2^{\text{brug}}$$

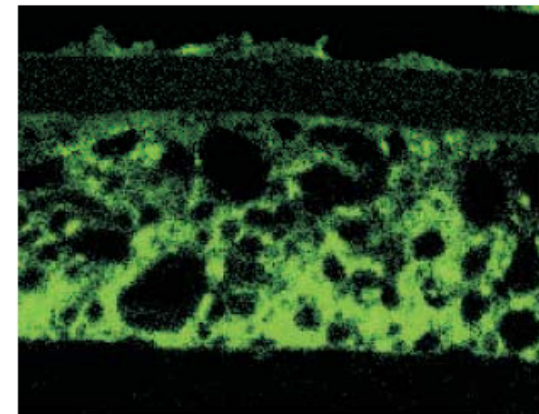
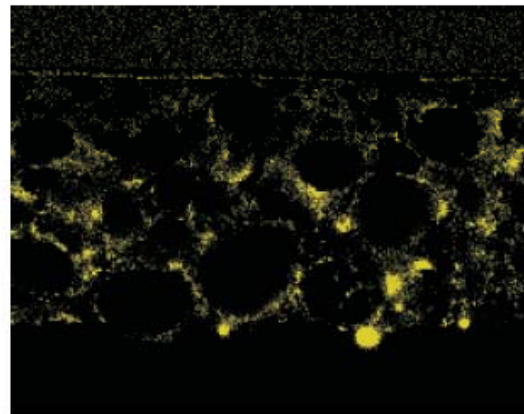


- Many different parameters **effect the same measured variable**, such as power or capacity fade
- It is usually not clearly defined **which parameter caused ageing of a certain cell at a given usage history** without opening the cells and performing sophisticated chemical analysis.
- By applying **special chemical and spectroscopic methods** (e.g. WDX analysis - shown for 0, 30, 3000 cycles - of increasing Fluorine deposition caused by cycling, to determine loss of active material and impedance rise), ageing mechanisms can be postulated and correlation effects can be worked out.

copper

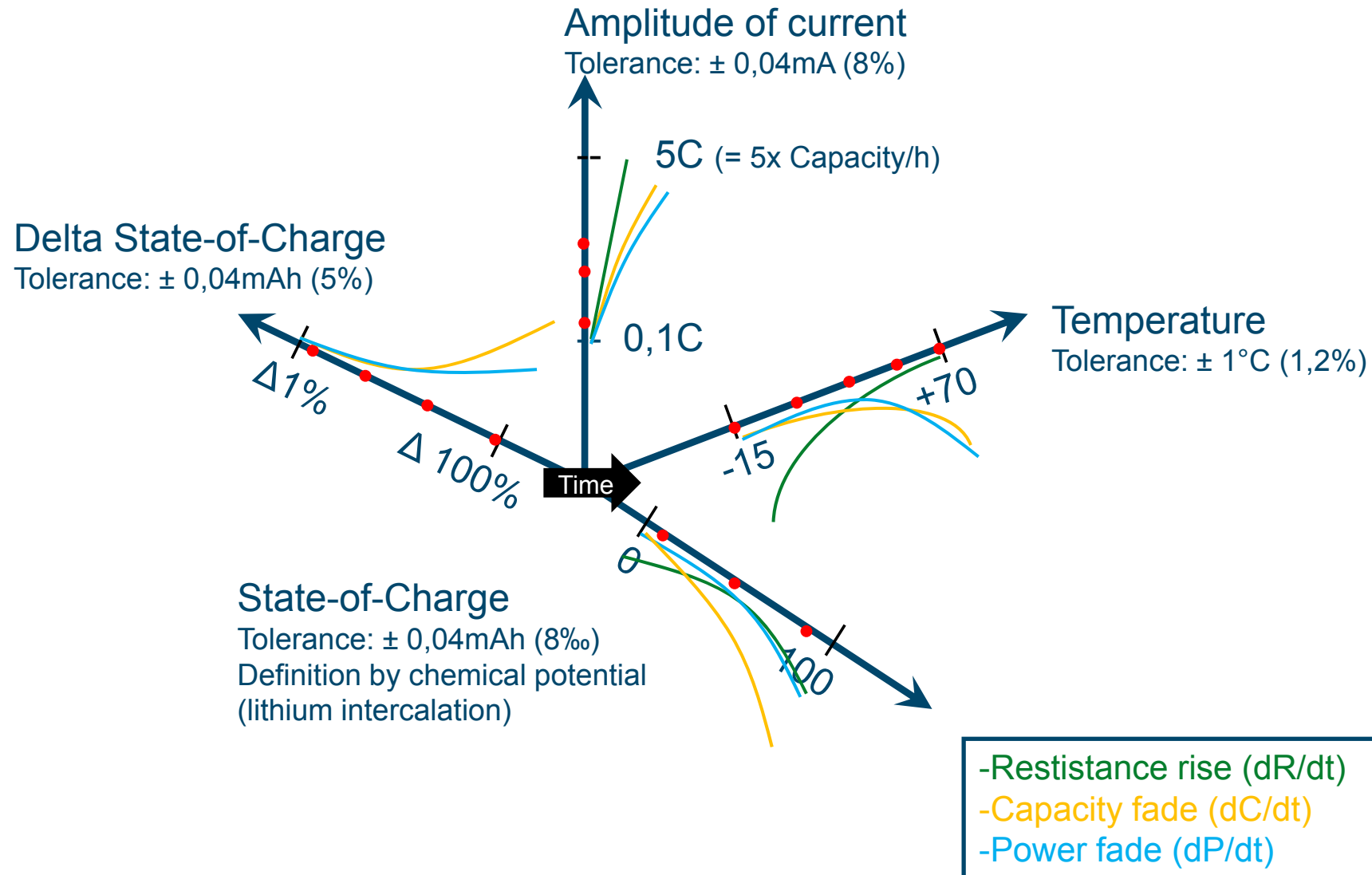


resin

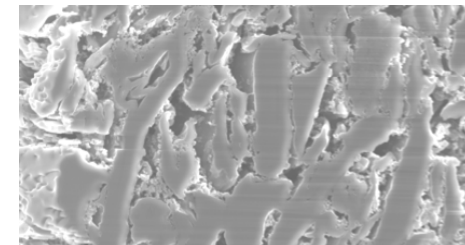


- Physics-based (electrochemical) models can be set up or extended

Ageing effect	Effect	Measurement	Influence factors
Collector corrosion (Cu)	Overpotential, power fade, impedance rise	Resistance, pulse constant	SoC↓↓
Contact loss of active material	Loss of active material, capacity fade	Capacitance	Cycling rate↑ DeltaSoC↑
Decomposition of binder	Loss of lithium, loss of electrode stability	Chemical composition	SoC↑ Temperature↑
Metallic lithium plating and subsequent electrolyte decomposition by metallic lithium	Capacity fade, power fade	Capacitance, pulse constant	Temperature↓, Cycling rate↑, Geometric misfits
Decomposition of electrolyte	Impedance rise, loss of lithium	Resistance, capacitance	Temperature↑ SoC↑, DeltaSoC↑
Changes in porosity due to volume changes, SEI formation and growth	Power fade, impedance rise, overpotentials	Chemical composition, capacitance, resistance, pulse constant	SoC↑, Cycling rate ↑, DeltaSoC↑
Changes in structure, changes in porosity	Capacity fade, power fade	Capacitance, REM, chemical composition	Temperature↑, SoC↑, DeltaSoC↑



- **Rate test, pulse test, driving cycles (e.g. NEDC), impedance measurements, ...**
- **Design of experiment**
 - DeltaSOC (0 to 100%) vs. SOC (0 to 100%)
 - Temperature (-20 to +70°C) vs. C-rate (0 to 5)
 - Limitation due to deceleration of chemical processes at low temperatures
 - DeltaSOC (0 to 100%) vs. C-rate (0 to 5)
 - Limitation caused by measurement instrumentation → inaccurate cycling (switching), predefined Delta SOC can not be maintained
 - Physics: at 0°C no change of SOC possible
- **Measurement quantities**
 - Resistance, capacitance, pulse response
 - Chemical composition → post mortem analyses
 - Structures via REM (2d images of porous electrodes)

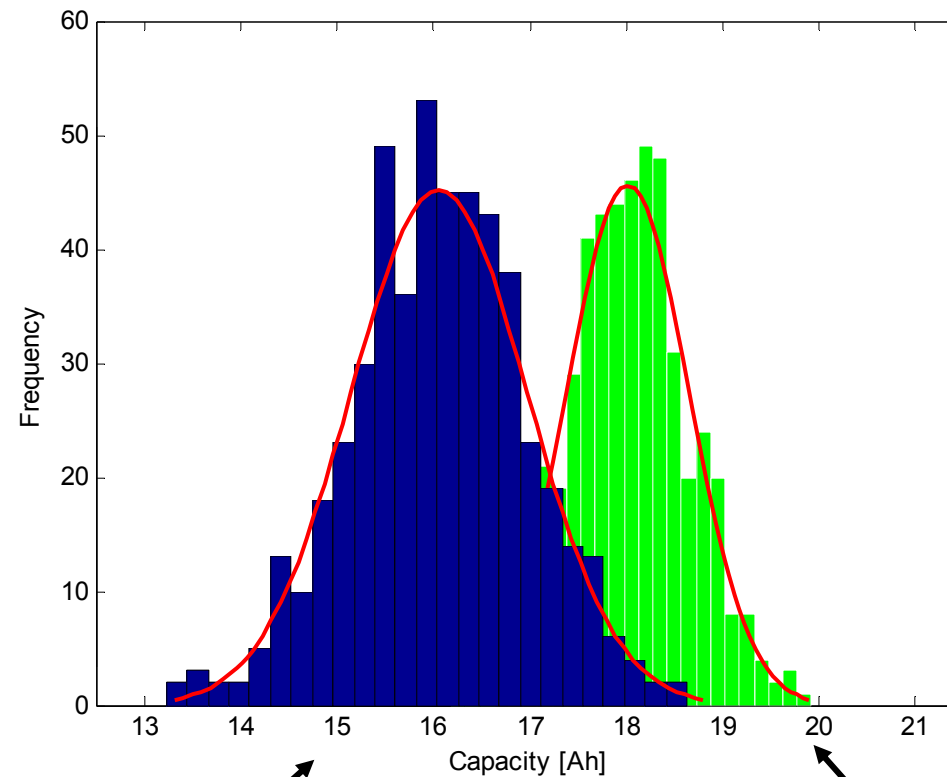


- **Manufacturing**

- Typical steps in cell production:

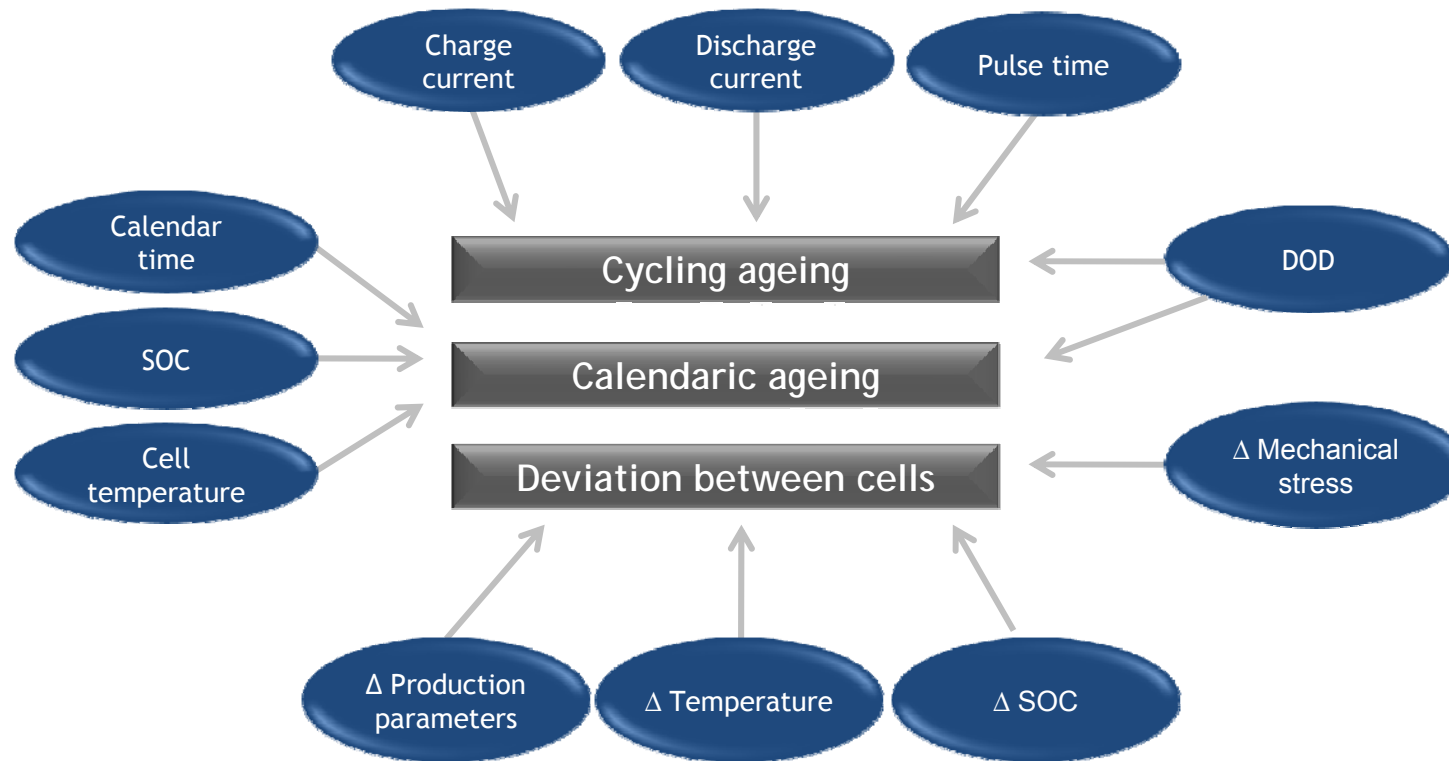
- weighing of cell components
 - Mixing
 - Coating (copper / aluminium foil)
 - Pressing of electrodes
 - Slitting
 - Jelly roll coiling (cathode, anode, separator)
 - Welding of current collectors
 - Dosing of electrolyte
 - Formation
 - Quality control

- **Characteristic cell parameter variations (e.g. cell capacity and internal resistance) due to variations of manufacturing steps (process tolerances, unwanted metal particles, water inclusions, geometries,...)**
- **leads to different behavior regarding ageing often even unknown by the manufacturer**

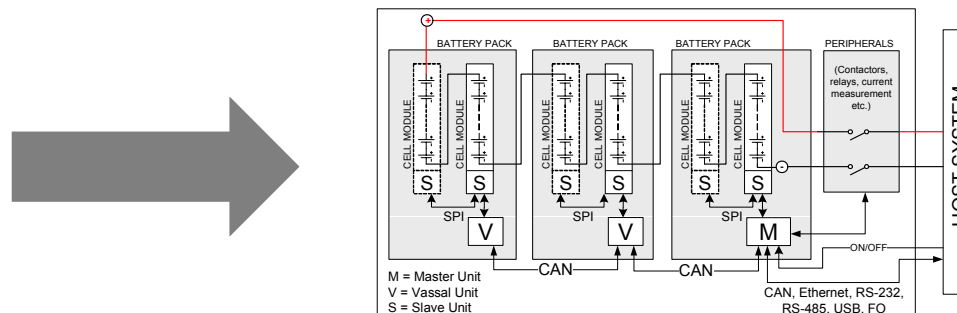


Variation after cycling (blue)
shift in mean
increase in standard deviation

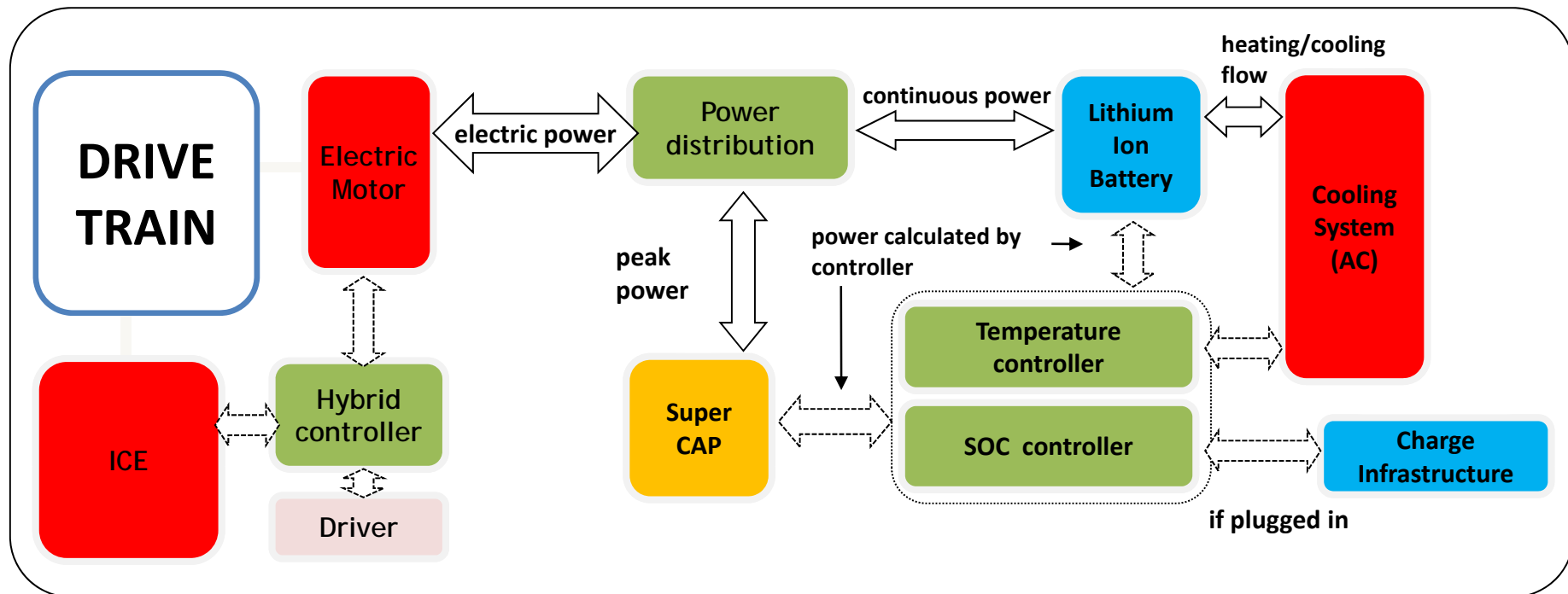
Cells after formation process (green)
scattering due to cell-to-cell variations



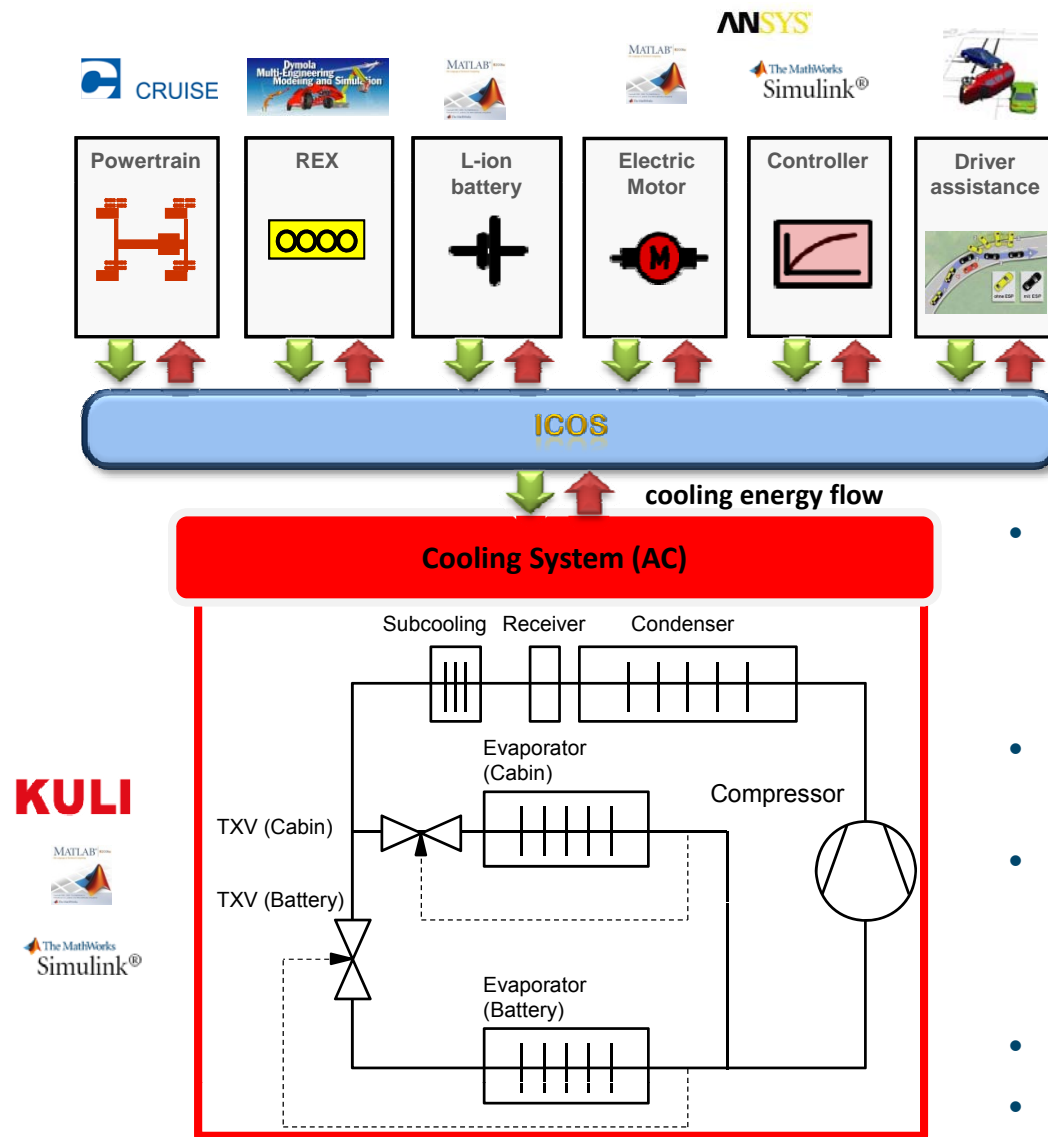
Battery management



SOC/SOH estimation and control
e.g. replacement of modules / package necessary?



- Hybrid architecture
- Lithium-ion battery
- Cascaded control



- Modeling using well-established domain-specific tools (Dymola, MATLAB/Simulink, Flowmaster, Kuli,...)
- Development of thermal operation strategies
- Cooling/heating strategies for battery
 - direct refrigerant cooling
 - coolant loop cooling
- cold start behavior
- predictive strategies

- Modeling of lithium-ion batteries is an active research field
- **No cell standard** (different materials, potentials, geometries, operation modes, energy and power densities,)
 - Models have to be **scaleable** in order to cover the existing range
- Different models can be used **for different statements**
 - **Polynomial and equivalent-circuit models** → energy management, model-based diagnosis, on-board parameter estimation,...
 - **Electrochemical models** → covering ageing aspects on an electrochemical basis, design support of cells (optimal design of internal cell structures), covering tolerances and manufacturing variations,...
- **Ageing effects** are not fully understood → strong interaction between electrochemistry, measurement, modeling, simulation, and estimation required.